

## The Hydrogenation of Hex-1-yne over Borohydride-reduced Catalysts. Evidence concerning the Mechanism of Reduction

By CHARLES ALLAN BROWN

(Chemistry Department, University of California, Berkeley, California; and †The Institute of Organic Chemistry, Syntex Research, 3401 Hillview Ave., Palo Alto, California 94304)

**Summary** In the hydrogenation of hex-1-yne over borohydride-reduced catalysts, hexane is formed in two distinct pathways, one not involving a free olefin intermediate.

As part of a systematic study of uses of the new borohydride-reduced catalysts,<sup>1-3</sup> the hydrogenation of terminal acetylenes was examined using hex-1-yne as a model compound. Of catalysts prepared from Group VIIIb metals,

only borohydride-reduced platinum, palladium, and nickel catalysts were appreciably active under model preparative conditions.‡ The observed rate of hydrogen uptake was appreciably slower for hex-1-yne than for a comparable olefin, oct-1-ene. This is particularly apparent in the case of rhodium, which is nearly inactive toward the alkyne yet is highly active toward alk-1-enes. This effect is shown in Table 1.

TABLE 1

Catalyst	Initial hydrogen uptake, ml. of H <sub>2</sub> at s.t.p. per min. <sup>a</sup>	
	Hex-1-yne	Oct-1-ene
Pt-BH <sub>3</sub> /C <sup>b</sup> .. .. .	22	90
Pd-BH <sub>4</sub> /C <sup>b</sup> .. .. .	36	90
Rh-BH <sub>4</sub> /C <sup>b</sup> .. .. .	2	72
P-1Ni <sup>c</sup> .. .. .	40	72
P-2Ni <sup>d</sup> .. .. .	62	72

<sup>a</sup> Separate hydrogenations of hex-1-yne and oct-1-ene.

<sup>b</sup> The carbon-supported borohydride reduced platinum metal catalysts.<sup>1</sup>

<sup>c</sup> Granular catalyst prepared in water.

<sup>d</sup> Colloidal catalyst prepared in alcohol.

† Present address.

‡ Hydrogenation of 40.0 mmoles of hex-1-yne over 0.20 mmole of noble metal or 5.0 mmoles of base metal in 50 ml of ethanol solution at 25°, 1 atm. The borohydride hydrogenation<sup>4</sup> with *in situ* generation of catalysts was employed throughout.

¶ No isomeric hexenes were detected even over the Pd-BH<sub>4</sub>/C catalyst which has been reported to produce considerable isomerization during hydrogenation of alk-1-enes.<sup>1</sup>

TABLE 2

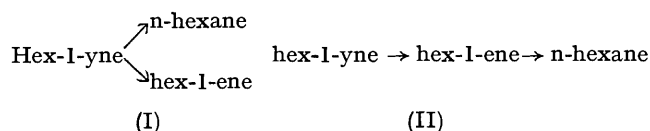
Catalyst	H <sub>2</sub> added, equiv. <sup>a</sup>	n-Hexane/hex-1-ene¶
Pt-BH <sub>4</sub> /C <sup>b</sup>	0.0 (extrap.)	0.21
	0.2	0.22
	0.5	0.24
	1.0	0.33
Pd-BH <sub>4</sub> /C <sup>b</sup>	0.5-1.0	0.03
P-1Ni <sup>c</sup>	0.0 (extrap.)-1.0	0.26
P-2Ni <sup>d</sup>	0.0 (extrap.)-1.0	0.27

<sup>a</sup> 2.0 equiv. required for hex-1-yne → hexane.

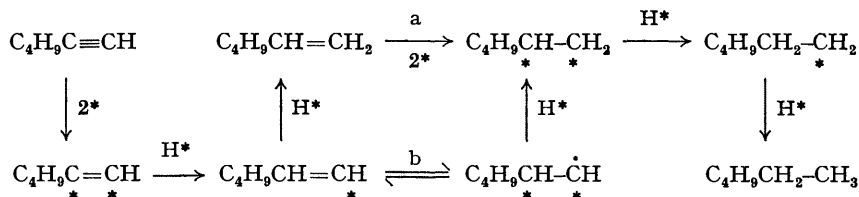
<sup>b,c,d</sup> See Table 1.

The reductions of hex-1-yne produce both hex-1-ene and hexane, even while unreacted alkyne remains; however, the proportions vary appreciably, as shown in Table 2. Only palladium is highly selective for hex-1-ene formation;

however, in general selectivity is considerably higher than might be expected from the independent hydrogenations. These results clearly suggest two pathways for the formation of hex-1-ene and n-hexane.



Pathway (I) requires a constant hexane: hexene ratio, with hexane produced even at the very beginning of the reaction when little or no hex-1-ene is present. Pathway (II) requires that the hexane: hexene ratio should increase from zero as the reaction proceeds and the hexene:hexyne ratio increases.\*\* P-INi, P-2Ni, and possibly Pd-BH<sub>4</sub>/C apparently catalyze by mechanism (I). Pt-BH<sub>4</sub>/C operates by a combination of (I) and (II); an appreciable hexane: hexene ratio is present from the beginning, yet the ratio increases as the reaction proceeds. These results are explained by the following mechanism.



(Received, November 11th, 1969; Com. 1720.)

\*\* Selectivity from (I) has been termed "mechanistic selectivity"; that from (II), "thermodynamic selectivity."<sup>5</sup>

†† Some question still remains as to whether these materials contain boron as an occluded solid, amorphous mixture, or definite stoichiometric boride.<sup>8</sup>

<sup>1</sup> H. C. Brown and C. A. Brown, *Tetrahedron*, 1966, *Suppl.* 8, *Part I*, 129.

<sup>2</sup> C. A. Brown and H. C. Brown, *J. Amer. Chem. Soc.*, 1963, **85**, 1003.

<sup>3</sup> H. C. Brown and C. A. Brown, *J. Amer. Chem. Soc.*, 1963, **85**, 1004.

<sup>4</sup> C. A. Brown and H. C. Brown, *J. Org. Chem.*, 1966, **31**, 3989. A commercial model of the apparatus was obtained from Delmar Scientific Laboratories, 317 Madison St., Maywood, Illinois, U.S.A.

<sup>5</sup> G. C. Bond, "Catalysis by Metals," Section 7.24, Academic Press, New York, 1962.

<sup>6</sup> Ref. 5, p. 294.

<sup>7</sup> (a) R. L. Augustine, "Catalytic Hydrogenation," Marcel Dekker, New York, 1967, p. 70; (b) P. N. Rylander, "Catalytic Hydrogenation over Platinum Metals," Academic Press, New York, 1967, pp. 62-67, and references therein.

<sup>8</sup> (a) C.-Y. Chen, H. Yamamoto, and T. Kuan, *Chem. and Pharm. Bull. (Japan)*, 1969, **17**, 1287; A. M. Taber, B. D. Polkovnikov, N. N. Mal'tseva, V. I. Mikheeva, and A. A. Balandin, *Doklady Akad. Nauk S.S.S.R.*, 1963, **152**, 119; (c) R. Paul, P. Buisson, and N. Joseph, *Compt. rend.*, 1951, **232**, 627; H. Narcus, *Plating*, 1967, **54**, 380; K. N. Mochalov, N. V. Tremasov, and Kh. V. Shifrin, *Trudy Kazansk. khim. Tekhnol. Inst.*, 1964, **33**, 95; (*Chem. Abs.*, 1966, **64**, 18,930g).